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## Rational Design of Etchants for Electroless Porous Silicon Formation

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From fundamental considerations of the surface chemistry of Si etching in fluoride solutions as well as pore formation and propagation, we develop a mechanistic understanding of what must be known for rational development of etchants: (1) an acidic fluoride solution because the presence of  $\text{OH}^-$  promotes step flow etching, (2) sufficiently high fluoride concentration compared to the oxidant concentration, (3) the oxidant must be able to inject holes into the Si valance band at a sufficient rate, hence  $E^\circ > -0.7$  V is required, (4) oxide formation needs to be slow or nonexistent so as to avoid the formation of a uniform oxide and associated electropolishing, (5) reduction of the oxidant must lead to soluble products, (6) film homogeneity is enhanced if the oxidant's half-reaction does not evolve gas, and finally (7) the net etching reaction has to be sufficiently anisotropic to support pore nucleation and propagation.

### Introduction

Stain etching of silicon is an electroless process (1, 2) that results in the formation of a nanocrystalline porous silicon (por-Si) layer, which can exhibit visible photoluminescence. By far the most common stain etchant is composed of an aqueous mixture of nitric acid and hydrofluoric acid. This is somewhat unfortunate as the reduction of  $\text{HNO}_3(\text{aq})$  is extremely complex and leads to the formation of various gaseous nitrogen oxides. The complexity and disadvantages of the nitric acid system have led to the conclusion that stain etching is irreproducible and capable of only producing inhomogeneous porous silicon layers that are less than 1  $\mu\text{m}$  thick (3). In this report we show that a deeper understanding of the processes that lead to electroless porous silicon formation allow us to rationally develop etchants with vastly superior characteristics as compared to the  $\text{HNO}_3 + \text{HF}$  system.

Using the rules derived by Kolasinski (1, 4), we have developed (5-9) new formulations of stain etchants that utilize  $\text{Fe}^{3+}$ ,  $\text{VO}_2^+$  and  $\text{Ce}^{4+}$  as the oxidant. These new formulations get around many of the problems associated with common nitrate/nitrite based stain etchants. The new formulations need no "activation", exhibit short if any induction time, produce homogeneous films and are quite reproducible. Film thicknesses of 10–20  $\mu\text{m}$  are easily obtained in as little as 60 min of etching (4).

The combination of infrared (FTIR) and cross section measurements yields complimentary information because FTIR interrogates both the chemical state of the surface and the surface area, while the cross section measures thickness. In  $\text{HF} + \text{V}_2\text{O}_5$  solutions, Kolasinski et al. (6) have shown that rate of film growth depends strongly on the oxidant and fluoride concentration. Addition of ethanol greatly decreases the etch rate and changes the pore morphology from a mixture of {100} + {110} planes to

predominantly {100} planes (6). A plot of thickness vs. etch time in aqueous solutions evolves from a quadratic to a linear dependence. Kolasinski and Yadvlovskiy developed a model in which pores with a uniform diameter nucleate randomly, initially grow rapidly before slowing to grow at a constant rate after saturation of the number of pores. The pore density increases linearly with time before saturation, causing a transition from a quadratic to a linear growth rate phase. This model simultaneously fits both the short time and long time behavior of the thickness and surface area for the  $V_2O_5$  etchant. Here we show that the nonlinear behavior of the film growth rate in  $Fe^{3+}$  solutions also follows this model. In addition we make quantitative comparisons of the hole injection rate in  $V_2O_5$  as compared to  $Fe^{3+}$  etchants.

### Experimental

Formation of por-Si by stain etching has been studied with infrared spectroscopy (FTIR), photoluminescence (PL) and scanning electron microscopy (SEM). Si(100) (*p*-type prime grade, 14–22  $\Omega$  cm resistivity),  $V_2O_5$  (Fisher certified grade),  $FeCl_3 \cdot 6H_2O$  (Fisher purified), and HF (JT Baker 48–51% analytical grade) were used. All etchants were aqueous with no added alcohol or surfactant. Samples were rinsed in 1:1 water/ethanol then ethanol (three times), and dried in a stream of Ar. Scanning electron microscopy (SEM) was performed with an FEI Quanta 400 ESEM. Fourier transform infrared spectroscopy (FTIR) was performed with a Nicolet Protégé 460. IR spectra were recorded with a diffuse reflectance attachment purged with dry  $N_2$  at a resolution of  $4\text{ cm}^{-1}$  by averaging 512 scans. A planar hydrogen-terminated surface created by etching a polished Si(100) wafer in 50% HF for 5 min was used for a reference spectrum.

### Results

Roughly  $1\text{ cm}^2$  substrates were etched in  $V_2O_5 + HF$  or  $FeCl_3 \cdot 6H_2O + HF$  and the surface area and thickness were followed as a function of etch time. The results are shown in Fig. 1 below. Note that the integrated IR absorption peak area is plotted in these figures. As discussed previously [6], this peak area is proportional to the true surface area; however, we have not determined the proportionality constant to arrive at the absolute magnitude.

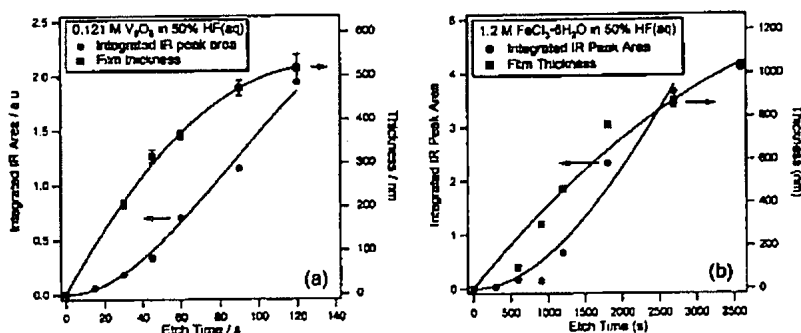


Figure 1 Thickness and integrated IR peak area versus time for porous films formed in (a)  $V_2O_5 + HF(aq)$  and (b)  $FeCl_3 \cdot 6H_2O + HF(aq)$ . The peak area is proportional to surface area.

## Discussion

Kolasinski and Yadlovskiy have previously analyzed the increase in surface area and thickness of por-Si film formed in  $V_2O_5 + HF$  solutions (5). They developed a model similar to that of Brumhead et al. (10), who proposed that film formation begins when fast developing pores nucleate and propagate from the surface into the bulk. During the nonlinear growth rate phase, the number of pores increases until the density reaches a saturation value that achieves carrier depletion in the nanoscale-width pore walls. We model the porous layer as being composed of an array of cylinders oriented perpendicular to the exterior surface of the film. The thickness increases quadratically in time during the initial portion of film formation

$$h = k_0 t + k_1 t^2 \quad [1]$$

as shown in Fig. 1. If the number of pores  $N$  increases linearly in time according to

$$N = k_2 t, \quad [2]$$

then the surface area  $A$  of  $N$  cylinders in a film with thickness greater than their radius,  $h \gg r$  is given by

$$A = \pi r (k_2 t) (k_0 t + k_1 t^2) = k_2 t (k_0 t + k_1 t^2). \quad [3]$$

The constants  $k_0$  and  $k_1$  are determined uniquely from the  $h$  vs.  $t$  data and the constant  $k_2$  is then determined independently from the FTIR data. The derivative of Eq. [1] yields the linear etch rate

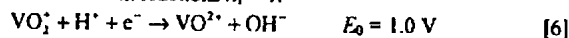
$$R_s = dh/dt = k_0 + 2k_1 t. \quad [4]$$

The constant  $k_0$ , therefore, is equal to the etch rate at time  $t = 0$ , which is not influenced by diffusion through the layer and represents a good quantity to quantitatively compare the efficacy of various oxidants at inducing por-Si formation. For the 0.121 M  $V_2O_5$  solution we find that the initial etch rate is  $R_{s,0} = 7.52 \pm 0.19 \text{ nm s}^{-1}$  and for the 1.2 M  $FeCl_3 \cdot 6H_2O$  solution  $R_{s,0} = 0.42 \pm 0.06 \text{ nm s}^{-1}$ .

Previously we have introduced the reactive sticking probability  $s_R$  as a measure of the efficiency of charge transfer between the Si and the oxidant (6). The reactive sticking coefficient is a measure of the probability that a collision of an oxidant with the surface leads to hole injection and then removal of a silicon atom. The etch rate is determined by the rate of hole injection (11, 12). Theoretically one Si atom is etched for each hole injected. In practice, many of the holes are lost to recombination or other nonetching related processes. The initial reactive sticking coefficient  $s_{R,0}$  is given by the ratio of the number of atoms etched to the number of collision of the oxidant with the surface, and can be written as

$$s_{R,0} = \frac{R_{s,0} \rho_A \epsilon}{n_i Z_w} = 7.923 \times 10^{23} \frac{R_{s,0} \epsilon M^{1/2}}{n_i c}, \quad [5]$$

where the porosity is  $\epsilon$ ,  $\rho_A$  is the atomic density of Si,  $Z_w$  the collision frequency of the oxidant,  $n_i$  the number of holes transferred per collision,  $c$  the concentration in  $\text{m}^{-3}$  of the oxidant, and  $M$  its molar mass in  $\text{g mol}^{-1}$ . The porosity of our films is roughly 0.8 based on reflectometry measurements. For both reactions  $n_i = 1$ :



For a 0.121 mol  $L^{-1}$  solution of  $V_2O_5$  in 50% HF, assuming that all of the  $V_2O_5$  dissolved to produce  $VO_2^+$ , the reactive charge transfer probability was  $s_{R,0} = 3.0 \times 10^{-3}$ . The reactive charge transfer probability is related to the charge transfer probability by

$$s_{R,0} = P_R i_0 \quad [8]$$

where  $P_R$  is the survival probability of the hole, that is, one minus the probability that the hole is lost to nonetching related relaxation. The reactive charge transfer probability was very low either because very few holes are injected per collision of  $\text{VO}_2^+$  with the surface and/or because the vast majority of the injected holes were lost to relaxation. For a  $1.2 \text{ mol L}^{-1}$  solution of  $\text{Fe}^{3+}$ , it is unclear what the solution phase species is. Most likely the  $\text{Fe(III)}$  is octahedrally coordinated in a complex of the form  $[\text{Fe}(\text{H}_2\text{O})_6\text{Cl}_n]^{3-n}$  with  $n = 0-3$  (13). The uncertainty in the mass leads to some uncertainty in the reactive charge transfer probability, which can nonetheless be estimated as  $s_{R,0} = 5 \times 10^{-10}$ .

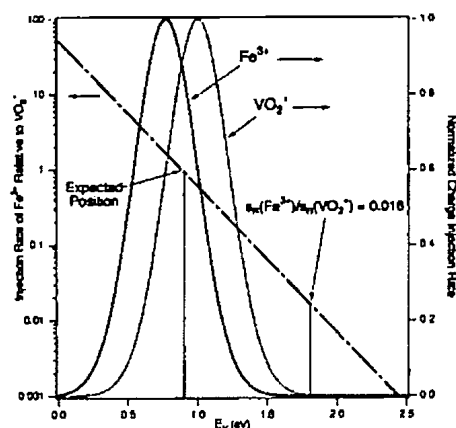


Figure 2. Calculated normalized rates of charge injection for  $\text{Fe}^{3+}$  and  $\text{VO}_2^+$  (right axis) and the charge injection rate of  $\text{Fe}^{3+}$  relative to that of  $\text{VO}_2^+$  (left axis).

The equilibrium charge transfer probability via the valence band is given by (14)

$$i_s = k_v^- (N_v - p_s^0) \exp\left[-(E_{ox}^+ - E_v) / 4\lambda k_B T\right] \quad [9]$$

where  $k_v^-$  a rate constant,  $N_v$  the density of states at the valence band edge,  $p_s^0$  the concentration of holes at the surface, the reorganization energy  $\lambda$ , position of acceptor level  $E_{ox}^+$ , position of the valence band maximum (VBM)  $E_v$ , absolute temperature  $T$  and  $k_B$  the Boltzmann constant must all be specified. The first three parameters should be independent of the oxidant in the solution because the surface is H-terminated in both cases and any effective doping changes caused by  $\text{H}^+$  or  $\text{F}^-$  penetration into the depletion layer are not changed by the presence of the oxidant. Thus, the normalized hole injection rate depends only on the exponential term. Substituting  $\lambda = 1 \text{ eV}$  and  $T = 300 \text{ K}$ , the normalized hole injection rates for  $\text{Fe}^{3+}$  and  $\text{VO}_2^+$  can be calculated. The results of this calculation are shown in Fig. 2 as a function of the energy of the valence band maximum. If  $E_v = 0.9 \text{ V}$ , which is its position relative to the standard hydrogen electrode in 5 M HF (15), then on the basis of this calculation we would expect  $s_{R,0}(\text{Fe(III)})/s_{R,0}(\text{V(V)}) = 0.94$  assuming that  $P_R$  is the same in both instance. Since both  $\text{Fe(III)}$  and  $\text{V(V)}$  transfer holes into the surface through one-electron transfers, it seems likely that  $P_R$  should be approximately the same in both cases. However, the measured

value of  $s_{R,0}(\text{Fe(III)})/s_{R,0}(\text{V(V)})=0.016$ . Therefore, either the valence band maximum has been shifted to  $E_v = 1.81$  V (see Fig. 2) or else the rate at which holes are injected by Fe(III) is much lower than expected based on the Marcus theory expression in Eq. [9]. To help us answer this question we need to measure  $s_{R,0}$  for at least one other species. We have already demonstrated that Ce(IV) effectively produces por-Si (7, 16). We have also found that  $\text{HIO}_3$  etches Si in HF(aq) but that por-Si formation is hampered by precipitation.

Si atoms are removed according to the Gerischer mechanism (11, 17, 18). Conclusive evidence against formation of  $\text{SiO}_2$  (or suboxide) and chemical removal by HF is obtained by examination of bubble formation (5). In any mechanism of stain etching, such as the Turner mechanism, that involves an oxide intermediate the formation of bubbles can only result from reactions involving the oxidant. For example, when  $\text{HNO}_3$  is used as an oxidant various reductions result in the production of  $\text{NO}_x$ . All of the gas should be  $\text{NO}_x$  and not  $\text{H}_2$ . However, Kooij et al. (19) found that  $\text{H}_2$  is formed in a 4:1 ratio compared to  $\text{NO}_x$ . On the other hand, in the Gerischer mechanism  $\text{H}_2$  is formed from hydrolysis of an etch product and the counter reaction required for charge balance. These reactions need not occur where etching occurs; therefore, bubbles can form remotely, either in solution or on other parts of the crystal. This is exactly what we observed. Initially bubbles form on the edges of the crystal and along scratches in the surface. Unlike metals, Si is a poor catalyst for  $\text{H}_2$  production and; therefore, the bubbles form first and primarily at highly defective regions of the crystal.

### Conclusion

Rational formulation of stain etchants to produce films of nanocrystalline porous silicon is possible once the dynamics of porous film formation are understood (4). The guidelines for formulation are (i) an acidic fluoride solution because the presence of  $\text{OH}^-$  promotes step flow etching, (ii) sufficiently high fluoride concentration compared to the oxidant concentration, (iii) the oxidant must be able to inject holes into the Si valence band at a sufficient rate, hence  $E^\circ > -0.7$  V is required, (iv) oxide formation needs to be slow or nonexistent so as to avoid the formation of a uniform oxide and associated electropolishing, (v) reduction of the oxidant must lead to soluble products, (vi) film homogeneity is enhanced if the oxidant's half-reaction does not evolve gas, and finally (vii) the net etching reaction has to be sufficiently anisotropic to support pore nucleation and propagation. Here we report the first quantitative comparison of the efficacy of two different oxidants at inducing porous silicon formation. We find that the reactive charge transfer probability is  $s_{R,0} = 3 \times 10^{-8}$  for  $\text{VO}_2^+$  and  $s_{R,0} = 5 \times 10^{-10}$  for Fe(III). Further experiments are underway to determine whether the difference in efficacy can be ascribed to the dependence of the hole injection rate on the position of the valence band maximum or to significantly different hole survival probabilities subsequent to injection.

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